

Wet flue gas desulphurisation procedures and relevant solvents thermophysical properties determination

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Abstract

In order to mitigate climate change, the priority task is to reduce emissions of greenhouse gases, including sulfur oxides, from stationary power plants. The legal framework of the European Union has limited the allowable emissions of gases with harmful effects and fulfillment of this obligation is also ahead of the Republic of Serbia in the following years. In this paper the categorization of wet procedures for sulfur oxides removal is given. Wet procedure with the most widespread industrial application, lime/limestone process, has been described in detail. In addition, the procedures with chemical and physical absorption and solvent thermal regeneration, which recently gained more importance, have been presented. Experimentally determined thermophysical and transport properties of commercially used and alternative solvents, necessary for the equipment design and process optimization, are also given in the paper. The obtained values of densities and viscosities of pure chemicals - solvents, polyethylene glycol 200 (PEG 200), polyethylene glycol 400 (PEG 400), tetraethylene glycol dimethyl ether (TEGDMA), N-methyl-2-pyrrolidone (NMP) and dimethylaniline (DMA), measured at the atmospheric pressure, are presented as a function of temperature.

Keywords: removal of sulfur oxides, flue gases, thermal power plant, density, viscosity, climate change.

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The sulfur oxides, generated by combustion of fuels containing sulfur (coal, oil), are the greenhouse gases with indirect effect. It is well known that these gases have a harmful impact on the environment, causing the occurrence of acid rains and respiratory problems. The flue gas desulphurization (FGD) processes had no commercial application, until the importance to protect the environment was understood, and consequently, the national legal regulations were adopted [1,2].

The EU regulations limited emissions of greenhouse gases and developed strategies to adapt to climate change. Republic of Serbia is facing a number of obligations, including the reduction of emissions of greenhouse gases, in the process of joining the European Union. Having this in mind, the processes used for flue gas desulphurization gained its importance.

This paper gives an overview of wet processes used for the removal of sulfur oxides from stationary power plants. Wet processes can be classified in non-regenerative (once-through) and regenerative procedures. The most important among them and also the most

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common in general practice is non-regenerative lime/limestone process. In this process the alkaline mixture is a reagent and gypsum is a final product. In regenerative procedures, used solvent is thermally regenerated and circulated back to the process. Among the regenerative procedures the most widespread are dual alkali process, process of chemical absorption in amines and process of physical absorption in organic solvents. The regenerative processes are further divided into those whose final product is disposed on landfill, and those with a commercially useful product.

For computer simulations, equipment design and consequently implementation of FGD procedures, it is necessary to have reliable data on thermophysical and transport properties of potential solvents. This paper presents experimentally determined densities (ρ) and viscosities (η) of pure solvents, polyethyleneglycol 200 (PEG 200), polyethyleneglycol 400 (PEG 400), tetraethylene glycol dimethyl ether (TEGDME), N-methyl-2-pyrrolidone (NMP) and dimethylaniline (DMA), in the temperature range from 288.15 to 323.15 K and at atmospheric pressure. Some of the above mentioned liquids have already found industrial application in the regenerative processes with organic solvents, while the others are suggested as alternative absorbents due to

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their favourable environmental impact, low toxicity or suitable physical and chemical properties.

Wet FGD processes

As stated above wet FGD processes can be classified into regenerative and once-through. Unlike once-through procedures, the regenerative processes include solvent regeneration stage. Based on the records of flue gases desulphurization processes on thermal power plants in the US, about 90% [3] of the applied procedures are once-through. Wet lime/limestone process has been used in about 78% [3] of plants in the US, and still is the most widespread FGD technology, with gypsum as the final, commercially valuable byproduct.

A general flow diagram of the non-regenerative FGD process is shown in Figure 1. The main part of the unit is the absorber, where the flue gas containing SO_2 is brought to contact with alkaline slurry. Before alkaline slurry enters the absorber, the sorbent solid particles are crushed (at desired particle size) in a crushing station. This is inevitable step, since crushing of the solid particles will increase dissolution rate in the preparation tank. The alkaline slurry is then fed to the reaction tank and transported to the top of the absorber, usually constructed as a spray tower or tray tower. The most common configuration of the absorber is vertical with counterflow of the phases, where the flue gas containing SO_2 is flowing upwards, and set of nozzles spray alkaline slurry (lime/limestone) downwards. In the process of removing SO_2 , two mechanisms take place, the sorption in the absorber and chemical reaction with the alkaline slurry in the reaction tank.

Lime/limestone process

Lime/limestone is by far the most common FGD process. The method was patented by Eschellman in 1909. The first commercial application of lime process was in London, England, and the first unit of the Battersea Power Station was put into operation in 1931. This once-through process used small amount of chalk added to water from River Thames as solvent. Many modern and improved lime/limestone processes [3,4] were based on this process.

Babcock & Wilcox Power Generation Group developed wet flue gas desulfurization systems based on standard lime/limestone process [5]. The reagent is an alkaline mixture of lime (calcium oxide (CaO) and calcium hydroxide (Ca(OH)_2)) or limestone (calcium carbonate (CaCO_3)) in water. The alkaline mixture as a reagent is introduced in absorber and brought into contact with flue gases containing SO_2 . Insoluble sulfates and sulfites (CaSO_4 and CaSO_3) formed in the reaction are removed as sludge. Gas, purified after passing through the separator, is released to the atmosphere. Used sludge from absorber is sent to the reaction tank, then to a dewatering stage where water is removed and finally to the landfill. The chemical reactions and process equipment are very similar regardless of whether the alkaline mixture of water with lime or limestone is used. Schematic representation of wet lime/limestone is similar to the general flow diagram presented in Figure 1.

For some applications, and under particular operating conditions, it is allowed to leave sulfite to sulfate oxidation process intact, in so-called natural oxidation mode. For most applications, however, it is necessary

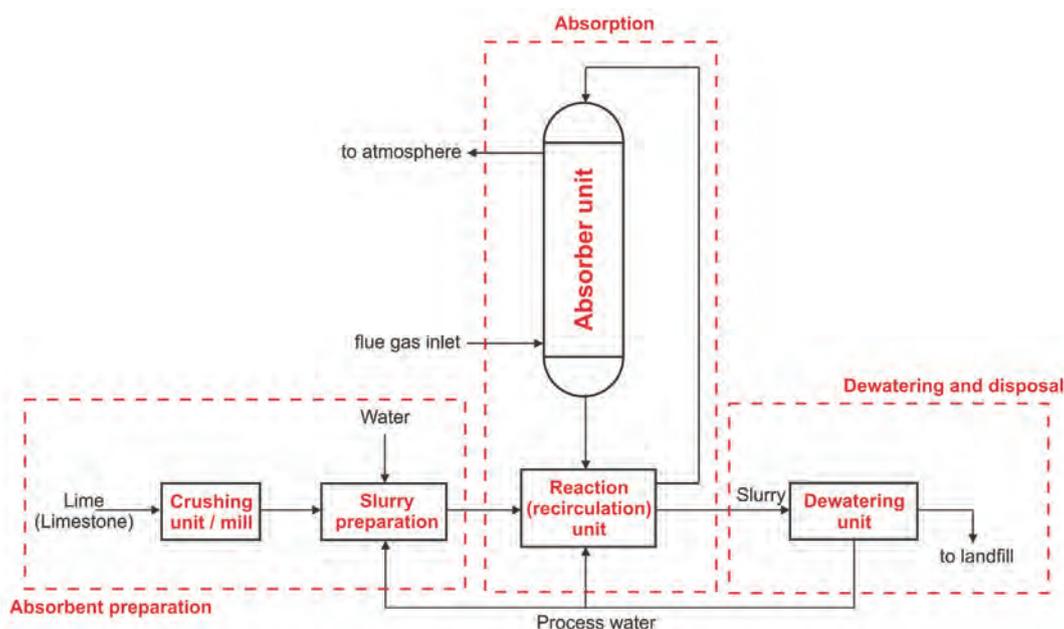


Figure 1. Wet FGD process – general flow diagram.

to control the oxidation process. One of the parameters that affects the process of oxidation in the absorber is liquid to gas phase flow rate ratio (L/G). Slurry pH is another process parameter that determines the amount of SO₂ removed. In order to improve reliability of the process it is necessary to control the oxidation process, so the limestone forced oxidation (LSFO) is most widespread subvariant. In order to prevent scaling problems, deposition of calcium sulfate - gypsum in the absorber, mist eliminator and piping, and to simplify slurry dewatering, air is usually blown through the absorbent slurry to force controlled oxidation outside the absorber. The air have to be blown through the reaction tank (in-situ oxidation) or through additional hold tank (ex-situ oxidation). Since market demand for gypsum has been reduced over the years and a wastewater treatment became a requirement, FGD technology with inhibited oxidation (LSIO) was offered as a solution.

In order to avoid scaling problems, sulfur and sodium thiosulfate emulsion could be added to the reaction tank, thus reducing oxidation rate below 15%. This variant of the process can be used with various reagents, lime, limestone, magnesium-enhanced lime and sodium. The advantages of LSIO are low investment and reagent costs and no necessity for wastewater treatment, which lead to lower overall operational costs.

Another sub-variety of lime/limestone procedure is a process enhanced by the presence of magnesium. As a sorbent, lime sludge is used, which is a mixture of water, lime and 5–8% magnesium oxide, or a mixture of water, lime and dolomite lime (with about 20% magnesium oxide). The enhanced process is very efficient compared to classic procedure and the final product is high-quality gypsum.

Since limestone is less reactive than lime, it requires slightly modified process equipment. The advantage of limestone compared to lime is in its market value (about 3 times cheaper than lime) which makes it more acceptable for use in large systems.

Wet lime/limestone process parameters are: flue gas velocity (residence time) through the absorber, L/G

ratio, lime/limestone milk pH value, SO_x concentration and solid particles concentration. Flue gas velocity through the absorber depends on the type of absorber. For absorber with countercurrent flow, increasing the speed of the flue gases, can lead to lower SO₂ removal efficiency. Required alkalinity of the process rises with the increase of L/G ratio. Efficiency of the process is influenced by pH value, while the concentration of particles and their residence time in the tank affect the reliability of the process. Typical values of concentration of solids in the mixture are 10–15% by weight, while the residence time of solids in the tank is 12–14 h. Higher values of these parameters can lead to unwanted particles' deposition in the equipment.

Removal efficiency for standard wet lime/limestone process is in range from about 60 to 97%, while for subvariety of enhanced lime/limestone process with magnesium, SO₂ removal efficiency can be increased to 99%. Basic operational parameters for lime/limestone systems on utility boilers in United States are given in Table 1.

Dual alkali process

Process name is derived due to presence of two types of components during absorption. Dual alkali process uses alkaline solution based on sodium as sorbent. Process also includes a stage of sorbent regeneration in which limestone is used. Calcium sulfite and sulfate formed in this stage are separated as sludge, while the regenerated sodium solution is reused in the absorption step (Figure 2). The chemistry of the process is very similar to the lime/limestone process.

Sodium-based solution (NaOH, Na₂CO₃ and Na₂SO₃) is brought into contact with the flue gas in the absorber. The used liquid solution is transported to the reactor within regeneration step, where the mixing with limestone, formation of calcium salts and sorbent regeneration take place. The sludge from the reactor is directed to the clarifier or thickener where it is filtered, water washed and emptied from the bottom. The regenerated sodium solution is sent to a mixing tank where sodium chemical compounds (soda ash or caustic soda) and water are added, and directed back to the absorber.

Table 1. Basic operational parameters for lime/limestone systems on utility boilers in US [3]

Alkaline mixture	Company/plant name	Power, MW	Fly ash control	Sulphur content in coal, %	L/G ratio, l/m ³
Water + CaO	Columbus & Southern Ohio Electric/ Conesville #5	411	Electrostatic precipitator	4.7	6.7
	Duquesne Light/Elrama	510		2.2	5.3
	Utah Power & Light/Hunter #1, Hunter #2	400		0.6	5.7
Water + CaCO ₃	Alabama Electric/Tombigbee #2, Tombigbee #3	255		1.2	9.4
	Commonwealth Edison/Powerton	450		3.5	8.0

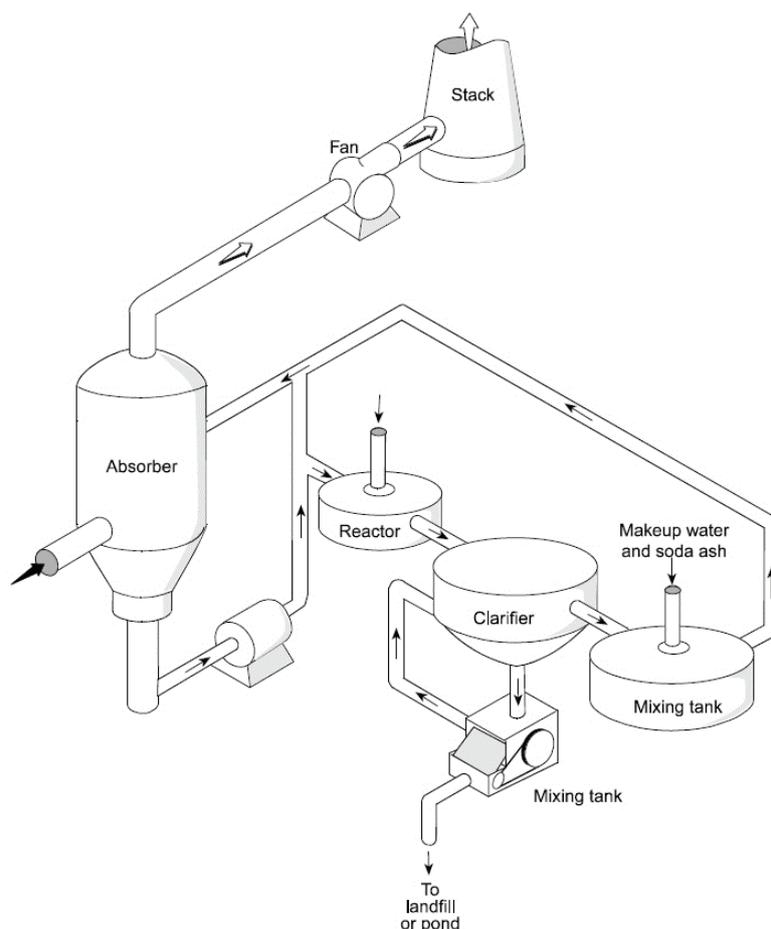


Figure 2. Schematic representation of the dual alkali process [3].

An alkaline solution of sodium is more efficient than lime/limestone solution. The required liquid to gas flow rate ratio (L/G) is much lower compared to the lime/limestone process, as can be concluded from Tables 1 and 2. Due to the lower L/G ratio, the process equipment is smaller in size. The process efficiency is about 95%. As a result of good solubility of sulfur oxides in sodium based alkaline solution, problems such as corrosion, erosion and deposit formation inside the equipment and installation are avoided.

Basic operational data for systems using dual alkali FGD process on utility boilers in the United States are given in Table 2 [3].

Amine processes with thermal regeneration

Processes based on chemical absorption in amines, already have applications for purification of outgoing

gases from smelters (with SO₂ content higher than 3.5%). Three aromatic amines, dimethylaniline (DMA), xylidine and toulidine, are commonly used as sorbents. DMA has a lower boiling point than the other two, a higher vapor pressure and its losses during the absorption process are higher. Xylidine is preferable than toulidine, due to its higher boiling point, however it has some undesirable properties. For low SO₂ concentrations, a mixture of xylidine and water as sorbent is more suitable, while for higher SO₂ concentrations, DMA is more appropriate. The examples of amine processes with thermal regeneration that already found commercial application are Sulphidine process, ASARCO process, Dow process and CANSOLV process. This paper briefly describes the CANSOLV process.

CANSOLV process [6], owned by Cansolv Technologies Incorporated, A Shell Global Solutions Company,

Table 2. Operational data for systems using dual alkali FGD process on utility boilers in the US [3]

Company/plant name	Power, MW	Fly ash control	Sulphur content in coal, %	L/G ratio, l/m ³
Central Illinois Public Service/Newton #1	617	Electrostatic	2.5	1.3
Louisville Gas & Electric/Cane Run #6	299	precipitator	4.8	1.3
Southern Indiana Gas & Electric/A.B. Brown #1	265		3.6	1.3

schematically is presented on Figure 3. It has a wide commercial application for purification of outgoing gases in industrial and utility boilers, smelters, refineries and chemical plants. The process has two steps, absorption and amine regeneration step. Flue gases come in contact with the amine solution in counter-current absorber, and treated gas exits with lower SO₂ content. Rich amine solution (with high absorbed SO₂ content) flows to the regeneration stage, and comes out as lean amine (with a lower sulfur content). Lean amine solution is regenerated by indirect steam stripping, clean SO₂ is set aside, dried and transported to sulfuric acid production unit. Lean amine leaves the regeneration unit and returns to the absorption unit.

CANSOLV process advantages are:

- Final products have its market value (pure SO₂, sulfur and sulphuric acid).
- The process does not produce solid waste.
- Low investment and operating costs.
- High flexibility in terms of gas flow rate fluctuations and SO₂ concentration in flue gases.

Physical (organic) solvent processes

Processes with organic solvents are among the most cost-effective and efficient processes for purification of flue gases with high or fluctuating SO_x content. Some

organic solvents have excellent selectivity towards SO₂, in relation to other flue gas components (N₂, O₂ and CO₂). Physical solvent for SO₂ removal should have temperature dependent solubility, high selectivity to SO₂, high chemical and thermal stability, low vapor pressure, should be environmentally friendly, not harmful to human health and cost effective. Solubility of SO₂ increases almost linearly with the increase of the physical solvent partial pressure, while solubility trend in chemical solvents has minimal growth or in some cases near zero.

Advantages of physical solvents in relation to chemical solvents are:

- Cost-effective process (lower energy requirements for solvent regeneration).
- Lack of heat released due to the chemical reactions.
- Useful and commercially valuable product.

Solinox process developed by the Linde AG group, is a practical application of the physical absorption in organic solvents. In United States Solinox process is offered by Lotepro Corporation, using tetraethylene-glycol dimethylether for SO₂ removal. Detailed description of the process and operating data from plants purifying flue gas streams that emanate from lead and

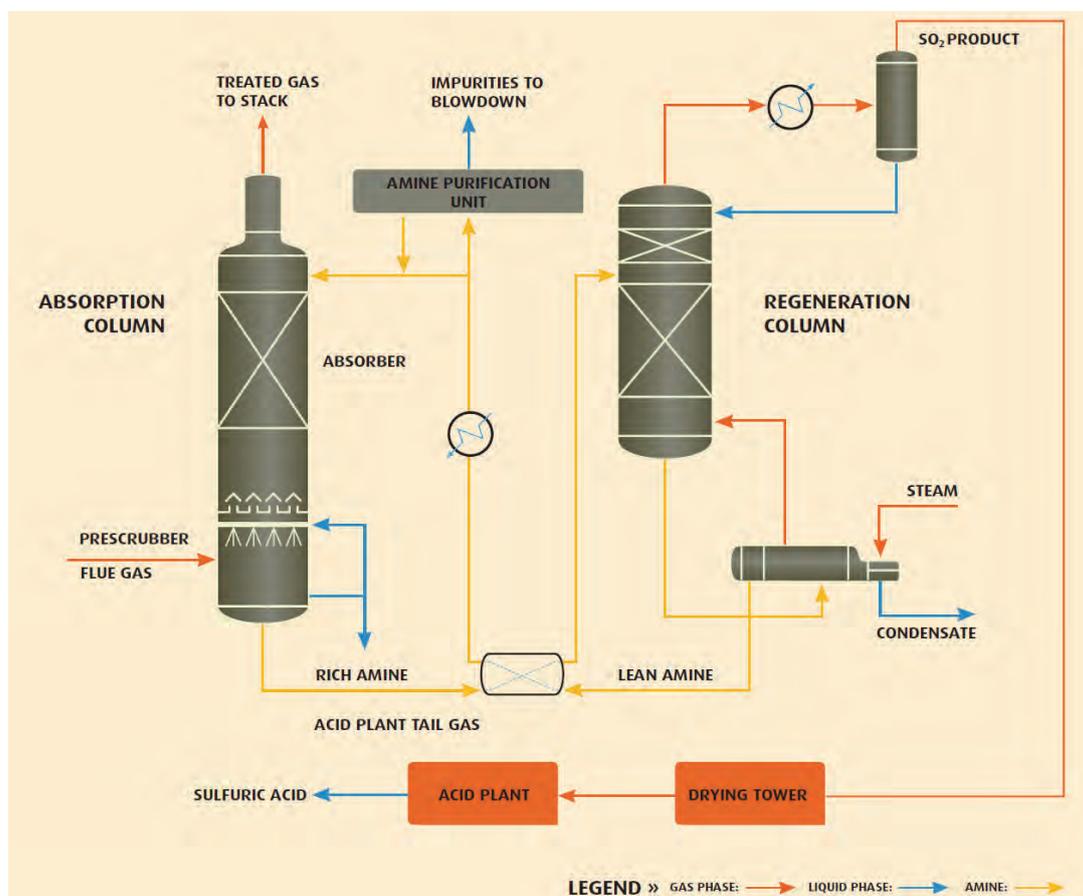


Figure 3. CANSOLV process, schematic representation [6].

zinc smelters is given by Sporer [7]. Before entering the absorber, flue gases have to be water washed, in order to lower the flue gas temperature and remove the impurities. The specific feature of this procedure is that it can remove hydrocarbons from outgoing gases, within the requirements for the air pollution control. The obtained removal efficiency for the process is 95–99.3%. Basic Solinox process has absorption and regeneration stage. The absorption stage takes place in countercurrent absorber, while regeneration stage (for separation of SO₂ from the solvent) takes place in countercurrent stripper with a reboiler.

However, investigations have shown that selectivity of TEGDME to sulfur dioxide is not satisfactory [8] and NMP as an alternative solvent has been proposed. Industrially, NMP has already been applied in Lurgi's Purisol process with excellent results in selective desulfurization of flue gasses from oil refineries and power plants.

As an alternative to above mentioned solvents several polymers, including PEG 200 and PEG 400, have been investigated [9]. The main advantages of PEG for desulfurization processes are high solubility and desorption capability for SO₂ which lead to lower energy requirements for absorption and regeneration processes.

Ionic liquids have been recently suggested as physical solvents for FGD processes [10–12]. Due to its favorable properties (high stability, low vapor pressure, excellent selectivity towards certain gases and non-toxicity) ionic liquids have found application in various separation processes. The preliminary investigations have shown that ionic liquids could also be used as an alternative to organic solvents in the processes of physical absorption and solvent regeneration.

Determination of thermodynamic and transport properties

In order to develop an absorption process for flue gases desulfurization and to set a numerical case for computer process simulation or work on equipment design, it is necessary to have reliable data on chemical, physical and transport properties of potential solvents. In this work the experimental densities and viscosities of five potential solvents for SO₂ removal, PEG 200, PEG 400, TEGDME, NMP and DMA, are reported at ten temperatures (288.15, 293.15, 298.15, 303.15, 308.15, 313.15, 318.15, 323.15, 328.15 and 333.15 K) and atmospheric pressure.

PEG 200, PEG 400 (99.5 mass%), NMP (99.0 mass%), DMA were supplied by Merck and TEGDME (99.0 mass%) by Acros Organics. Chemicals were kept in dark bottles in an inert atmosphere, used without further purification and degassed just before a sample preparation.

Densities, ρ , of the pure substances were measured using an Anton Paar DMA 5000 digital vibrating U-tube densimeter (with automatic viscosity correction) having a stated accuracy of $\pm 5 \times 10^{-6}$ g·cm⁻³. The temperature in the cell was regulated to ± 0.001 K with a built in solid-state thermostat. Temperature in the cell was measured by means of two integrated Pt 100 platinum thermometers and temperature stability was better than ± 0.002 K. Calibration of the apparatus was performed daily using ambient air and Milipore quality water. The combined expanded uncertainty in the density is within $\pm 2 \times 10^{-5}$ g·cm⁻³ with a 0.95 level of confidence ($k \approx 2$).

Viscosities, η , of the pure substances were measured with a digital Anton Paar Stabinger viscometer (model SVM 3000/G2). The instrument contains two measuring cells; one of them is used for measuring the density of the sample. U-tube is filled with the sample liquid and excited to oscillate using magnetic coils. Density measurement is based on the relation between oscillation period and sample density. The other cell, used for dynamic viscosity measurements contains a straight tube filled with sample. The tube rotates at a constant speed. In this tube, centered by the centrifugal force, floats a measuring rotor made of low density material, with a built-in magnet. A rotating magnet in SVM 3000 induces an eddy current field with a speed dependant brake torque. Shortly after the start of the experiment the rotor reaches a constant speed determined by the equilibrium between the viscosity-dependent driving torque, proportional to the speed difference between the tube and the rotor, and the brake torque caused by eddy currents. The kinematic viscosity is calculated from the measured density and dynamic viscosity. The stated reproducibility of the dynamic viscosity and density measurements is 0.35% and 5×10^{-4} g·cm⁻³ in the temperature interval 288.15 to 333.15 K. The temperature in the cell was regulated to ± 0.01 K with a built in solid-state thermostat. The relative uncertainty in dynamic viscosity measurements was estimated to be within $\pm 0.8\%$.

RESULTS AND DISCUSSION

Experimental data of density (ρ) and viscosity (η) for pure chemicals PEG 200, PEG 400, TEGDME, NMP and DMA at ten temperatures, 288.15, 293.15, 298.15, 303.15, 308.15, 313.15, 318.15, 323.15, 328.15 and 333.15 K, and atmospheric pressure, are presented in Tables 3 and 4.

In Table 5, densities and dynamic viscosities of pure PEG 200, PEG 400, TEGDME, NMP and DMA have been compared with literature values at 298.15 and 303.15 K [13–24]. The agreement between literature and our experimental values is very good with differences less than 6.5×10^{-4} g·cm⁻³ for density measurements and

Table 3. Measured density values ($\rho / \text{g}\cdot\text{cm}^{-3}$) of pure PEG 200, PEG 400, TEGDME, NMP and DMA at atmospheric pressure

T / K	PEG 200	PEG 400	TEGDME	NMP	DMA
288.15	1.128778	1.13009	1.01563	1.037298	0.960062
293.15	1.124828	1.126001	1.010995	1.03284	0.955975
298.15	1.120865	1.121905	1.006359	1.028382	0.951878
303.15	1.116909	1.117802	1.001732	1.023925	0.947778
308.15	1.112945	1.113711	0.997104	1.019462	0.943669
313.15	1.108981	1.109622	0.992481	1.015	0.939552
318.15	1.105016	1.105536	0.987859	1.010533	0.935426
323.15	1.101043	1.101461	0.983234	1.006061	0.931291
328.15	1.097068	1.09739	0.978613	1.001583	0.927142
333.15	1.093088	1.093324	0.973989	0.997096	0.92298

Table 4. Measured viscosity values ($\eta / \text{mPa}\cdot\text{s}$) of pure PEG 200, PEG 400, TEGDME, NMP and DMA at atmospheric pressure

T/K	PEG 200	PEG 400	TEGDME	NMP	DMA
288.15	86.442	161.67	4.3415	1.9896	1.5247
293.15	64.815	119.54	3.8338	1.8232	1.403
298.15	49.724	90.582	3.3801	1.6795	1.2965
303.15	38.912	70.145	3.0042	1.5546	1.2035
308.15	31.006	55.365	2.6913	1.4443	1.1205
313.15	25.102	44.463	2.4258	1.3464	1.0462
318.15	20.602	36.262	2.1994	1.2593	0.97959
323.15	17.136	29.981	2.0063	1.1816	0.91971
328.15	14.424	25.097	1.8382	1.1099	0.86528
333.15	12.343	21.247	1.6914	1.0427	0.81953

Table 5. Densities ρ and dynamic viscosities η of pure components at atmospheric pressure

Component	T / K	$\rho / \text{g}\cdot\text{cm}^{-3}$		$\eta / \text{mPa}\cdot\text{s}$	
		Exp.	Lit.	Exp.	Lit.
PEG 200	298.15	1.120865	1.12098 [13]	49.724	48.157 [13]
PEG 400	298.15	1.121905	1.12249 [13] 1.12230 [14] 1.1218 [9] 1.12162 [15]	90.582	92.797 [13]
TEGDME	298.15	1.006359	1.0063 [16] 1.0067 [17] 1.0059 [18] 1.00653 [19]	3.3801	3.394 [16] 3.313 [18]
NMP	298.15	1.028382	1.02872 [20] 1.0283 [21]	1.6795	1.656 [20] 1.67 [21]
DMA	303.15	0.947778	0.9484 [22] 0.948 [23] 0.94833 [24]	1.2035	1.174 [23] 1.170 [24]

within 7×10^{-2} mPa·s for viscosity measurements of less viscous fluids. The differences between experimental and literature values of viscosity are somewhat higher for more viscous fluids but still under 3% deviation.

Densities of pure components decrease with temperature increase, as expected. Measured density data

show linear temperature dependence and can be correlated with linear expression (1):

$$\rho = A_0 + A_1 T \quad (1)$$

With the temperature increase viscosities behave in the same manner as densities, their values decrease

with temperature increase and can be correlated with polynomial expression (2):

$$\eta = B_0 + B_1T + B_2T^2 + B_3T^3 \quad (2)$$

Parameters A_0 , A_1 , B_0 , B_1 , B_2 and B_3 in expressions (1) and (2) are presented in Table 6.

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Table 6. Polynomial parameters A_p and B_p for pure solvents (expressions (1) and (2))

Property	A_0, B_0	A_1, B_1	B_2	B_3
PEG 200				
$\rho / \text{g}\cdot\text{cm}^{-3}$	1.3573	-0.0008	-	-
$\eta / \text{mPa}\cdot\text{s}$	33739	-310.01	0.9516	-0.001
PEG 400				
$\rho / \text{g}\cdot\text{cm}^{-3}$	1.3656	-0.0008	-	-
$\eta / \text{mPa}\cdot\text{s}$	68033	-626.54	1.9271	-0.002
TEGDME				
$\rho / \text{g}\cdot\text{cm}^{-3}$	1.2822	-0.0009	-	-
$\eta / \text{mPa}\cdot\text{s}$	440.97	-3.8412	0.0113	$-1 \cdot 10^{-5}$
NMP				
$\rho / \text{g}\cdot\text{cm}^{-3}$	1.2947	-0.0009	-	-
$\eta / \text{mPa}\cdot\text{s}$	125.22	-1.0819	0.0032	$-3 \cdot 10^{-6}$
DMA				
$\rho / \text{g}\cdot\text{cm}^{-3}$	1.1975	-0.0008	-	-
$\eta / \text{mPa}\cdot\text{s}$	72.575	-0.6057	0.0017	$-1.7 \cdot 10^{-6}$

CONCLUSION

In the years to come, Republic of Serbia will be faced with the need and obligations to reduce emissions of greenhouse gases, including sulfur oxides. In view of this fact, particular attention has to be focused on emissions from major polluters – the stationary power plants.

In this paper, review of wet flue gas desulphurization technologies has been presented. The most common technology for flue gas desulfurization is wet lime/limestone process. With development of flue gas desulphurization technology, wet procedures with solvent regeneration attract more attention, because of their advantages, in terms of efficiency, solvent use and environmental impact. Among regenerative procedures the most widespread are dual alkali process and processes based on absorption in amines or absorption in organic solvents.

The transport properties of potential solvents for FGD processes are of great importance for computer simulation and equipment design. Thermophysical and transport properties (density and viscosity) of pure solvents, PEG 200, PEG 400, TEGDME, NMP and DMA have been measured and presented in the paper.

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IZVOD

PREGLED MOKRIH POSTUPAKA ZA ODSUMPORAVANJE DIMNIH GASOVA I ODREĐIVANJE TERMOFIZIČKIH SVOJSTAVA NJIMA ODGOVARAJUĆIH RASTVARAČA

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Za ublažavanje klimatskih promena, neophodno je izvršiti smanjenje emisija gasova sa efektom staklene bašte među koje spadaju i sumporni oksidi iz stacionarnih termoenergetskih postrojenja. Ublažavanje promena je uslovljeno zakonskim okvirom Evropske Unije. Ispunjenje ove obaveze je i pred Republikom Srbijom u narednim godinama. S obzirom na prioritete i aktuelnost navedene problematike, u radu je data kategorizacija mokrih postupaka za uklanjanje sumpornih oksida iz dimnih gasova iz termoelektrana i prikazane su karakteristike odgovarajućih solvenata za regenerativne postupke. Opisan je u praksi najzastupljeniji mokri krečni postupak. Predstavljene su postupci sa termalnom regeneracijom solventa zasnovani na hemijskoj ili fizičkoj apsorpciji, koji u poslednje vreme imaju sve veći značaj. Prikazani su rezultati eksperimentalnog određivanja termofizičkih svojstva komercijalno primenjenih i alternativnih solvenata, koja su od primarnog značaja za projektovanje opreme i optimizaciju procesa. Izmerene vrednosti gustine i viskoznosti čistih rastvarača, polietilenglikol 200 i 400 (PEG 200 i PEG 400), tetraetilenglikola–dimetil-etar (TEGDME), *N*-metil-2-pirolidona (NMP) i dimetilanilina (DMA), na atmosferskom pritisku, predstavljene su u funkciji temperature.

Ključne reči: Uklanjanje sumpornih oksida • Dimni gasovi • Termoelektrana • Gustina • Viskoznost • Klimatske promene